

cine as fuel. It was seen that Mg(NO3)2.6H2O and Al(NO3)3.9H2O show different behavior with respect to urea and glycine . Also the variation of fuel to oxidizer (F/O) ratio was studied . The study was carried out for leaner to richer fuel ratios. In the case of MgAl2O4 combustion synthesis results were achieved when fuel mixture (urea and glycine) were used. The useof fuel mixtures allowed the formation of pure, nano-crystalline MgAl2O4 directly from the combustion reaction. The effect of fuel mixture ratios was investigated by variation of the ratios in which the fuel was taken . The later product was characterized by XRay-diffraction analysis . The nanoscaled images where taken by SEM (Scanning Electron Microscope) of the powder being produced.

Introduction

Magnesium aluminate spinel (MgAl₂O₄) is one of the widely used materials[1-3].various method like sol-gel, coprecipitation etc have being used to produce oxides In the MgO-Al₂O₂ system the only compound that forms as a result of the reaction between the two oxides is MgA-I₂O₄, called spinel. Magnesium Aluminate has a low density (3.58 g/cm3). Due to its significant properties – high melting point, 2135 °C, low thermal conductivity, low thermal expansion coefficient, high mechanical strength both at room temperature and elevated temperature, good thermal shock resistance and good chemical insipidness [1,4]. This is the result that all these properties of MgAl₂O₄ are successfully applied in various applications, like refractory bricks manufacturing for the cement and steel industry transparent windows, good resistance against chemicals and better strength at extreme high temperatures, military applications (armour materials, domes), humidity sensors, catalysts support, dentistry and nuclear technique [1]. The synthesis of MgAl₂O₄ with specific characteristics such as chemical homogeneity, high purity, low particle size and uniform size distribution depends considerably on preparation methods. As such, magnesium aluminate has been synthesized by various methods such as sol-gel, solid state, spray drying , co-precipitation , and freeze-drying. However, most of these methods are either complex or expensive which lower preparation of the nano-sized materials in a large scale as compared to the combustion or sol-gel synthesis [4-10]. Moreover, other disadvantages are the necessity of high temperature, inhomogeneity, and low surface area of the nano-sized products [4]. In this work, Here we have used the fuel to oxidizer variation for formation of Magnesium Aluminate (MgAl₂O₄) powder. In addition, fuel mixtures were also used to prepare $MgAl_2O_4$ and other oxide powders, e.g. $MgAl_2O_4$ from urea and glycine . Mixtures of urea and glycine were worked as fuel to synthesize nano scale MgAl₂O₄ powders via a solution combustion process. Moreover, the effects of urea and glycine addition on characteristics (e.g. particles size and specific surface area) of the powders were synthesized [2]. The further characterization was carried out by XRay-diffraction and SEM examinations.

Experimental procedure

A. Solution Combustion Synthesis (SCS) of Magnesium Aluminate (MgAl $_2O_4$) with Various Fuel to Oxidisers Ratios:

Analytical grade Aluminum Nitrate nonahydrate (Al (NO₃)₃·9H₂O), urea (CO (NH₂)₂), Glycine (NH₂CH₂COOH) were used as oxidizer and fuel respectively for SCS. These reactants are mixed in the required molar ratios with required amount as shown in Table.1 in a minimum volume of deionized water to obtain clear aqueous solutions. The solution is then kept in furnace preheated to 500°C. First thermal dehydration (at 100°C) takes place forming viscous solution, at 200°C the viscous liquids swelled and gets auto ignited, with the rapid evolution of a large volume of gases to produce voluminous powders. The nature of ignition depended on the fuel-to-oxidant ratio. The auto ignition of the precursor containing fuel-to-oxidant ratio according to the concept of propellant chemistry and fuelrich ratio was found to be more violent compared to the fuel-deficient precursor. Because the time for which the auto ignition exists is rather small (typically 5 s), Under the equilibrium conditions the standard reaction equation in this systems can be represented for all trivalent nitrates urea combustion (Where M=trivalent cation) for different fuel to oxidizer ratio as

For all Magnesium nitrate, Aluminium nitrate, urea, glycine combustion for different F/O ratios equation can be written as.

 $\begin{array}{l} \mathsf{Mg}(\mathsf{NO}_3)_2.6\mathsf{H}_2\mathsf{O}+2\mathsf{Al}(\mathsf{NO}_3)_3.9\mathsf{H}_2\mathsf{O}+4.44 \\ \mathsf{NH}_2\mathsf{CH}2\mathsf{COOH} \end{array} \rightarrow \\ \mathsf{MgAl}_2\mathsf{O}_4 + (4+2.22 \\ \emptyset)\mathsf{N}_2 + 8.88 \\ \mathsf{SCO}_2 + (24+11.1 \\ \emptyset)\mathsf{H}_2\mathsf{O} + \end{array}$

Here the ${\it 0}$ is the fuel to oxidizer equivalence ratio (not the urea to nitrate molar ratio) given by the formula

 $\frac{Fuel}{\text{oxidiser}} Ratio = \frac{\sum all \text{ oxidising and redusing elements in fuel}}{\sum all \text{ oxidising and redusing elements in oxidizer}}$

B.Solution Combustion Synthesis of $\mathrm{MgAl_2O_4}\,\mathrm{BY}\,\mathrm{MIXEDFU-ELS}$

MgAl₂O₄ synthesis has been considered to study the effect of nature of fuel, decomposition temperature difference of fuel and oxidizer, furnace temperature (in case of multi cationic nitrate fuel system) on SCS powders. The MgAl₂O₄ was prepared by using Magnesium nitrate, Aluminium nitrate, as oxidizers and urea, glycine as fuels and coded as in Table 6. Effect of mixed fuel also was studied by using reactants from Table 6. The reactants are mixed in distilled water in molar ratio and mass as shown in Table 6. These solutions, then kept in a furnace pre heated to 500°C. The combustion reaction characteristics are shown in table. Under the equilibrium conditions the standard reaction equation in these fuels- nitrate systems for preparation of MgA l_2O_4 by MIXED fuels can be represented as below

Mg(NO₃)₂.6H₂O+2Al(NO₃)₃.9H₂O+5NH₂CONH₂+1.11NH₂CH ₂COOH

→MgAl₂O₄ +7.22CO₂ +27.51H₂O +9.55N₂

 $\begin{array}{l} {\rm Mg(NO_{3})_{2}.6H_{2}O+2Al(NO_{3})_{3}.9H_{2}O+3NH_{2}CONH_{2}+2.44NH2C} \\ {\rm H2COOH} \end{array}$

→MgAl₂O₄+7.88CO₂+27.88H₂O+8.22N₂

Structural, Compositional and Micro-structural Analysis. X-ray diffraction (XRD)

X-ray diffraction studies were carried out for phase confirmation and for calculating crystallite size of the milled samples, using D8-Advance-Bruker machine with Cu-K_a (wavelength of Cu-K_a (λ) ~1.5406 Å) radiations for all the measurements. Ni filter was used to attenuate K_β lines. The crystallite size of powders was calculated using Scherrer's formula where an assumption was made that the particle is spherical in shape The Scherrer's formula gives

$$\beta \theta = \frac{k' \lambda}{d. COS \theta}$$
(3)

where, β_{θ} is the full width at half maximum (FWHM) of diffracted peaks in degrees, L stands for the liner dimension of particles in meters, θ refers to Bragg's angle in degrees and K' is the shape factor, generally known as a numerical constant and evaluated as 0.93 and depends on shape of crystallites. From this expression, it is clearly seen that diffracted beam gets broadened as the size of crystallite reduces. Silicon was used as an external standard for correction due to instrumental broadening.

Scanning electron microscope (SEM)

The surface morphology of powders and pellet samples was studied using scanning electron microscope a Cambridge, stereoscan-240. (ESEM –FEI, Quanta 200) and elemental compositional analysis was done using the attached energy dispersed analysis of X-rays (EDAX). The grain size of the chosen materials was seen clearly using FEG-SEM .All the samples studied were ceramic oxide insulator materials (non conductors).Grain size was estimated

using linear intercept method.

Thermodynamic Modeling

For comparing exothermicity of different fuels in reaction with the nitrates, enthalpy and adiabatic flame temperature of the reactions between urea and aluminum nitrate were calculated in the conditions:- Stoichiometric, Fuel lean and Fuel rich. Using the thermodynamic data for the various reactants and products listed in Table 2.2, the enthalpy of combustion and the theoretical adiabatic flame temperatures as a function of F/O ratio were approximately calculated by the following equations: using Mathematica software

$$\Delta H^{\circ} = (\Sigma n \Delta H^{\circ})_{\text{products}} - (\Sigma n \Delta H^{\circ})_{\text{reactant}}$$
(4)

Here ΔH° is the enthalpy of combustion reaction, Cp is the heat capacity of products.

Table1.Relevant thermodynamics data of reactants and products

Compound	∆H _f (kcal. mol ⁻¹)	c _p (cal.mol ⁻¹ .K ⁻¹)
MgAl ₂ O ₄	-547.38	-
Al(NO₃)₃· ©	-857.59	-
Zn(NO) ⋅6H O ©	-551.30	-
NH ₂ CONH ₂ ©	-79.71	-
NH,CH,COOH ©	-126.22	-
	100.0/	
CH ₃ CHNH ₂ COOH ©	-100.26	-
Ca (NO ₃) ₃ ·4H ₂ O ©	-509.64	-
Mg (NO₃)₃·6H₂O ©	-624.59	-
SiO ₂	-217.75	-
CaMgSi ₂ O ₆ ©	28.8	-
NH ₄ NO ₃	-87.37	-
Al ₂ O ₃ ©	-399.09	52.3+ 0.00774T
		33.3
		22.08 + 0.0089T
ZnO ©	-83.24	11.40 + 0.00145 <i>T</i> - 182400/ <i>T</i> ²
CO ₂ (g)	-94.051	10.34 + 0.00274 <i>T</i> – 195500/ <i>T</i> ²
NO ₂ (g)	7.93	8.8
N ₂ (g)	0	6.50 + 0.0010T
H ₂ O (g)	-57.796	$8.22 + 0.00015T + 0.0000134T^2$
H ₂ O (I)	-68.38	-
O ₂ (g)	0	8.27 + 0.000258T - 18770/T ²
©:crystalline; (g):gas; (l):liquid; (7):absolute temperature;		

RESULTS AND DISCUSSIONS

Solution Combustion Synthesis (SCS) of Magnesium Aluminate (MgAl $_{2}\mathrm{O}_{4}$) with Various F/O Ratios:

Considering the reaction of nitrates with the urea fuel the

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obtained results are ,

For fuel lean \emptyset <1, three compositions of fuel lean are \emptyset =0.4,0.8 and chemical equations are respectively (60%,20% fuel lean)

Ø=0.4,fuel lean

Mg(NO3)2.6H2O+2Al (NO₃)₃.9H₂O +2.66NH₂CONH₂

→ MgAl₂O₄+5N₂+2.66CO₂+29.32H₂O+6O₂

Ø=0.8,fuel lean

Mg(NO₃)₂.6H₂O +2Al (NO₃)₃.9H₂O +5.33NH₂CONH₂

→MgAl₂O₄+9.33N₂+5.33CO₂+34.66H₂O+2O₂

Fuel stoichiometric Ø=1

Mg(NO₃)₂.6H₂0 + 2Al (NO₃)₃.9H₂O +6.66NH₂CONH₂

 \rightarrow MgAl₂O₄+10.66N₂+6.66CO₂+37.32H₂O

Fuel rich Ø>1 Ø =1.2, 1.4, 1.6 (20%, 40%, 60% fuel rich) reaction equations are

 $Mg(NO_3)_2.6H_20 + 2AI(NO_3)_3.9H_2O + 8NH_2CONH_2$

→MgAl₂O₄+12 N₂+8 CO₂+40H₂O+2O₂

Mg(NO₃)₂.6H₂0 + 2AI (NO₃)₃.9H₂O + 9.33NH₂CONH₂

 \rightarrow MgAl₂O₄+13.33N₂+9.33CO₂+42.66H₂O+4O₂

 $Mg(NO_3)_2.6H_20 + 2AI(NO_3)_3.9H_2O + 10.66NH_2CONH_2$

→MgAl₂O₄+14.6N₂+10.66CO₂+45.32 H₂O+6O₂

The above equations are for complete combustion equations formed by assuming extra oxygen needed in fuel rich case is supplied by atmospheric air.

Table 2 . The required molar ratios with required amount of F/O ratios as shown below for Urea as fuel.

Fuel to oxi- dizer	Urea- nitrate molar	Mg (NO ₃₎₂ 6H ₂ O ²	Al (NO ₃) ₃ .9H ₂ O	Urea CO (NH)	Rect-ion type	Colour of pow-
ratio	ratio	(g)	(g)	(g)		der
0.4	1	5.12	15	3.2	No flame	white
0.8	1.5	5.12	15	6.4	No flame	white
1.0	2.5	5.12	15	8	flame	white
1.2	3.0	5.12	15	9.6	flame	white
1.4	3.5	5.12	15	11.20	flame	white
1.6	4	5.12	15	12.8	flame	white

From equation (1) for Magnesium nitrate , Aluminium nitrate ,urea combustion can be written in terms of Fueloxidizer ratio (Ø) as

 $\Delta H_{(Products)} = \Delta H_{(MgAl2O4)} + (4+6.66\%) * \Delta H_{(N2)} + 6.66\% * \Delta H_{(CO2)} + 6.6\% * \Delta H$

(24+13.32ø) *∆H_(H2O) +(10-10 ø))* ∆H_(O2)

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∆H_(Products)=-547.38+(4+6.66ø)*0+6.66ø*(-94.051)+ (24+13.32ø) *(-57.796) +(10-10 ø)*0

=- 547.38-626.37 ø-1387.104-769.84 ø

 $\Delta H_{(Products)} = -1934.484-1396.21 \text{ } \emptyset$

 $\Delta H_{(Reactants)} = \Delta H_{(Mg(NO3)2.6H2O)} + 2^{*} \Delta H_{(AI (NO3)3.9H2O)} + 6.66^{*} \Delta H_{(NH2CONH2)}$

 $\Delta H_{(Reactants)} = -624.59 + 2*(-857.59) + 6$

ΔH_(Reaction) =(-1934.484-1396.21 ø)-(-2339.77-530.8686 ø)

+6.66 ø *(-79.71)

 $\Delta H_{(Reactants)} = -2339.77-530.8686 \text{ } \emptyset$

 $\Delta H_{(\text{Reaction})} = \Delta H_{(\text{Products})} - \Delta H_{(\text{Reactants})}$ (from equation (4))

(5)

By considering the average Cp values of combustion products from

 $\begin{array}{l} Cp_{_{(Products)}} = Cp_{_{(MgAl2O4)}} + (~4+6.66 \varnothing) * Cp_{_{(N2)}} + ~6.66 \varnothing ~*~ Cp_{_{(CO2)}} + (~24+13.32 \varnothing) * Cp_{_{(H2O)}} ~+ (10\text{-}10 ~\varnothing) * ~Cp_{_{(O2)}} \end{array}$

Cp_(Products) =42.79+ (4+6.66ø) x6.961+6.66ø x8.87+ (24+13.32ø) x8.025+ (10-10 ø)x7.01

Cp=440.227+35.33ø

No of moles of gases/mole product=38+16.64ø (6)

Similarly for glycine as fuel ,the variation of fuel to oxidizer ratio was carried out and the results were obtained as follows

For fuel lean Ø<1, three compositions of fuel lean are Ø=0.4,0.8 and chemical equations are respectively (60%,20% fuel lean)

Ø=0.4, fuel lean

Mg(NO3)2.6H2O+2AI (NO₃)₃.9H₂O +1.77NH₂CH₂COOH

→ MgAl₂O₄+4.88N₂+3.54CO₂+28.42H₂O+6O₂

Ø=0.8,fuel lean

Mg(NO₃)₂.6H₂O +2Al (NO₃)₃.9H₂O +3.55NH₂CH₂COOH

→MgAl₂O₄+5.77N₂+7.1CO₂+32.87H₂O+2O₂

Fuel stoichiometric \emptyset =1

Mg(NO₃)₂.6H₂0 + 2AI (NO₃)₃.9H₂O +4.44NH₂CH₂COOH

→ MgAl₂O₄+6.22N₂+8.88CO₂+35H₂O

Fuel rich Ø>1 Ø =1.2, 1.4, 1.6 (20%, 40%, 60% fuel rich) reaction equations are,

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Mg(NO₃)₂.6H₂0 + 2AI (NO₃)₃.9H₂O + 6.22NH₂CH₂COOH

4O₂

Mg(NO_),.6H,0 + 2AI (NO_),.9H,0 + 7.11NH,CH,COOH

→ MgAl₂O₄+7.11N₂+12.44CO₂+39.55H₂O+

→MgAl₂O₄+7.55N₂+14.22CO₂+41.77H₂O+6O₂

Table 3 . The required molar ratios with required amount of F/O ratios as shown below for Glycine as fuel

Fuel to oxi- dizer ratio	Urea- nitrate molar ratio	Mg (NO ₃) ₂ . 6H ₂ O (g)	Al (NO ₃) ₃ .9H ₂ O (g)	Glycine NH ₂ CH- ₂ COOH (g)	Rect- ion type	Colour of powder
0.4	1	5.12	15	2.66	No flame	White
0.8	1.5	5.12	15	5.32	No flame	Brown-ish white
1.0	2.5	5.12	15	6.66	flame	Grey white
1.2	3.0	5.12	15	7.98	flame	grey
1.4	3.5	5.12	15	9.30	flame	Dark grey
1.6	4	5.12	15	10.64	flame	Black

Standard equation for Magnesium nitrate , Aluminium nitrate ,glycine combustion can be written in terms of Fueloxidizer ratio (Ø) as

Mg(NO₃)₂.6H₂O+2Al(NO₃)₃.9H₂O+4.44 øNH₂CH₂COOH

→MgAl₂O₄+(4+2.22ø)N₂+8.88øCO₂+(24+11.1ø)H₂0+(10-10 ø)O₂

 $\Delta H_{(Products)} = -1934.484-1476.7 \text{ }$

 $\Delta H_{(\text{Reactants})} = \Delta H_{(\text{Mg(NO3)2.6H2O)}} + 2^{*} \Delta H_{(\text{AI (NO3)3.9H2O)}} + 4.44^{*} \Delta H_{(\text{NH2CH2COOH})}$

 $\Delta H_{(Reactants)} = -624.59 + 2*(-857.59) + 4.44 ø *(-126.22)$

 $\Delta H_{(\text{Reactants})} = -2339.77-560.41 \text{ }$

 $\Delta H_{(Reaction)} = \Delta H_{(Products)} - \Delta H_{(Reactants)}$

 $\Delta H_{(\text{Reaction})} = (-1934.484 - 1476.7 \text{ ø}) - (-2339.77 - 560.41 \text{ ø})$

 $\Delta H_{(Reaction)} = 405.28-916.29 \ \text{\emptyset} \tag{7}$

By considering the average Cp values of combustion products from

 $\begin{array}{l} Cp_{(Products)} = Cp_{(MgAl2O4)} + (\ 4+2.22 \varnothing)^* Cp_{(N2)} + \ 8.88 \varnothing \ ^* \ Cp_{(CO2)} + (\ 24+11.1 \varnothing)^* Cp_{(H2O)} \ + (10-10 \ \varnothing)^* \ Cp_{(O2)} \end{array}$

Cp_(Products) =42.79+ (4+2.22ø) x6.961+8.88ø x8.87+ (24+11.1ø) x8.025+ (10-10 ø)x7.01 Cp=333.244+113.27ø

∆Cp= 333.244+113.27ø -98.83 ø =333.244-14.44ø

No of moles of gases/mole product=28+22.21ø (8)

The adiabatic flame temperature was calculate using formula $% \left({{{\rm{T}}_{{\rm{s}}}}_{{\rm{s}}}} \right)$

 $T_{ad} = To + (\Delta Hp - \Delta Hr) / C_{p}$ (9)

Table 4. Effect of Urea – Nitrate F/O ratio on adiabatic flame temperature, enthalpy of reaction, no of moles of gases evolved

Fuel/oxidiser	Enthalpy(∆H) Kcal/mol	Adiabatic flame temp (T _{ad}) °C	No gases evolved
0.4	59.065	467.71	44.65
0.8	-287.25	961.80	51.31
1.0	-460.06	1266.26	54.64
1.2	-634.1	1521.61	57.96
1.4	-806.98	1737.31	61.29
1.6	-979.79	1922.63	64.62

Table 5. Effect of Glycine– Nitrate F/O ratio on adiabatic flame temperature, enthalpy of reaction, number of moles of gases evolved

Fuel/oxidiser	Enthalpy(∆H) Kcal/mol	Adiabatic flame temp (T _{ad}) °C	No gases evolved
0.4	38.21	411.55	36.88
0.8	-262.95	1089.23	45.76
1.0	-458.37	1360.45	50.21
1.2	-690	1727.57	54.65
1.4	-879.34	1989.78	59.09
1.6	-1060.07	2203.16	63.53

B.Solution Combustion Synthesis (SCS) of Magnesium Aluminate (MgAl₂O₄) with MIXED FUELS:

The MgAl₂O₄ was prepared by using Magnesium nitrate, Aluminium nitrate, as oxidizers and urea, glycine as fuels. Effect of mixed fuel also was studied by using variation of fuel mixture as in Table.6. The fuels (reactants) are mixed in deionized water in molar ratio and mass as shown in Table. 6. These solutions, then kept in a furnace pre heated to 500°C. The combustion reaction characteristics are shown in Table.6. Under the equilibrium conditions the standard reaction equation in these fuels- nitrate systems for preparation of MgAl₂O₄ by mixed fuels can be represented as below

 $\begin{array}{l} \mathsf{Mg}(\mathsf{NO}_3)_2.6\mathsf{H}_2\mathsf{O}+2\mathsf{AI}(\mathsf{NO}_3)_3.9\mathsf{H}_2\mathsf{O}+6.6\mathsf{NH}_2\mathsf{CONH}_2\\ \boldsymbol{\rightarrow}\mathsf{MgAl}_2\mathsf{O}_4+6.6\mathsf{CO}_2+28.2\mathsf{H}_2\mathsf{O}+10.6\mathsf{N}_2 \end{array}$

 $\begin{array}{lll} \mathsf{Mg}(\mathsf{NO}_3)_2.6\mathsf{H}_2\mathsf{O} & +2\mathsf{AI} & (\mathsf{NO}_3)_3.9\mathsf{H}_2\mathsf{O} + 4.4\mathsf{NH}_2\mathsf{CH}_2\mathsf{COOH} \\ \boldsymbol{\rightarrow}\mathsf{Mg}\mathsf{AI2O4} + 8.8\mathsf{CO}_2 + 26\mathsf{H}_2\mathsf{O} + 6.2\mathsf{N}_2 \end{array}$

 $\begin{array}{l} {\rm Mg(NO_3)_2.6H_2O+2Al(NO_3)_3.9H_2O+5NH_2CONH_2+1.11NH_2CH}\\ _2{\rm COOH} \twoheadrightarrow {\rm MgAl_2O_4+7.22CO_2+27.51H_2O} + 9.55N_2 \end{array}$

 $\begin{array}{l} \mathsf{Mg}(\mathsf{NO}_3)_2.6\mathsf{H}_2\mathsf{O}+2\mathsf{Al}(\mathsf{NO}_3)_3.9\mathsf{H}_2\mathsf{O}+3\mathsf{NH}_2\mathsf{CONH}_2+2.44\mathsf{NH2C}\\ \mathsf{H2COOH} \rightarrow \mathsf{MgAl}_2\mathsf{O}_4+7.88\mathsf{CO}_2+27.88\mathsf{H}_2\mathsf{O}+8.22\mathsf{N}_2 \end{array}$

Table 6.A mount of fuel and oxidizer, used for the combustion reaction to produce ${\rm MgAl_2O_4}$ by mixed fuel approach.

		Sample code	Mg (NO3)2 (g)	Al (NO3)3 (g)	Fuel Urea (g)	Fuel gly- cine (g)	Obta- ined Powder (g)
,	Д	Mg- 5U+1.11G	5.12	15	6	1.66	2.89
	В	Mg- 3U+2.44G	5.12	15	3.6	3.66	2.76

CHARECTERIZATION RESULTS

X –ray characterization :

Figure 9 shows XRD pattern of the synthesized powder for Mixture of fuels . It shows the formation of pure crystalline MgAl₂O₄ phase confirmed by comparing the peaks with standard peaks of (JCPDS card number 75-1796) with little impurity peak of Al₂O₃ (JCPDS card no 82-1468) at 20 value of 43.35°. The formation of phase pure crystalline magnesium aluminate is confirmed by comparing the peaks with standard peaks of JCPDS card number for the mixed fuels. The percentage of magnesium aluminate phase increases as deviation goes from stoichiometric to fuel rich and fuel lean. It was also observed that there was a formation of impurities in case of lean mixtures .For fuel rich region even though the enthalpies of reactions are higher than that of fuel lean but the amount of gases produced in the reactions are more than the stoichiometric composition so those gases take the more amount energy. It was noted in Figure 10 that the formation of Mg₂N₄ and MgC_a(JCPDS card no 47-1456) takes place at lower temperature due to incomplete combustion. Figure.9 shows XRD pattern of the as synthesized MgAl₂O₄ powder formed by using mixed fuels of urea and glycine maintaining stoichiometric conditionThe furnace temperature maintained was 500°C. But here when taken with aluminium nitrate and using urea and glycine mixed fuel could able to form the Magnesiunm Aluminate. The crystallite size(d) was calculated using Scherer formula (3)

Table 7 . Representing the crystallite size in nano meters

Sr.no	$\beta_{\theta} =$ full width at half maximum (FWHM)	θ	Cos θ	d (nm)
1	0.334	9.62	0.98	24.3
2	0.246	15.78	0.96	33.4
3	0.250	18.57	0.94	33.5
4	0.266	22.55	0.92	32.2
5	0.294	29.83	0.86	31.2
6	0.30	32.76	0.84	31.1

Scanning Electron Microscope (SEM):

Figure 10 , 11 and 12 show the SEM images of $MgAl_2O_4$ of porous morphology with sphere like agglomerates ranging from 10 to100 nm. The agglomerates are porous due to escaped number of moles of gases released in combustion reaction . Some particles are sintered to form big hard aggregates of 1-5µm. Some isolated 100nm seized particles are also seen in $MgAl_2O_4$ powder. The formation of $MgAl_2O_4$ when used with mixture of fules shows that temperature given was enough to help the formation of the spinel powder. Associated gas evolution results in highly porous structure as the amount of gas increases agglomerates are more likely to break and form the porous structure as seen in the images.

FIGURES AND GRAPHS



Figure 1.Muffle Furnace setup.



Figure 2. Clear aqueous solution of fuel and oxidizer mixture in solution combustion synthesis used.



Figure 3. Different powders formed after scs with fuel to oxidizer (F/O) variation when urea was used as fuel.



Figure 4 . Different powders formed after scs with fuel to oxidizer (F/O) variation when glycine was used as fuel.









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Figure 5. Phases of powder formation during Solution Sombustion Synthesis.



Figure 6. Graph representing the enthalpy vs F/O ratio for



Figure 7. : Graph of fuel /oxidizer ratio on measured flame temperature.

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Figure 8. Graph of number of moles of gases released as a function of fuel to oxidizer ratio .



Figure 9. XRD pattern of Magnesium Aluminate powders synthesized by solution combustion synthesis by mixed fuels



Figure 10. . XRD pattern of powders at lean fuel by solution combustion synthesis



Figure 10. SEM image showing nano MgAl₂O₄ Spinels



Figure 11. SEM image showing Porousity developed due to escaped gases at fuel rich in variation of F/O ratio.



Figure 12. SEM image showing agglomerates of MgA- I_2O_4 powder.

v. conclusions

This paper is a study on solution combustion synthesis by variation of fuel to oxidizer ratio and by mixed fuels . The end results are promising and the characterization results prove that the formation of Magnesium Aluminate can be carried out at low temperatures (500 °C) using two or more fuels together . More precisely it is a low cost and newer method of producing oxides .

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